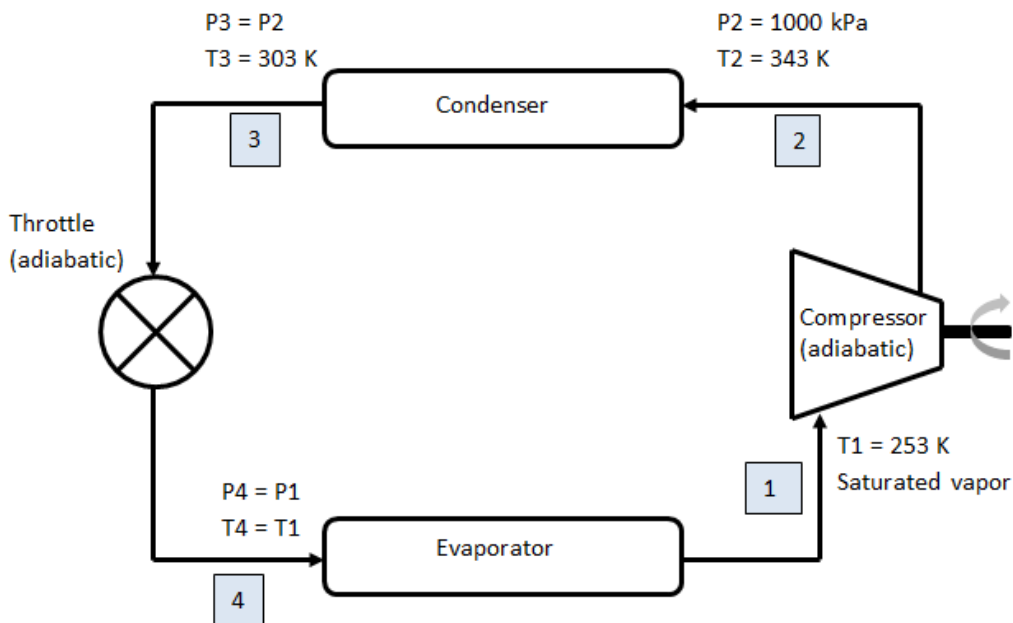


Analysis of a Vapor-Compression Refrigeration Cycle

Introduction

This application analyzes this refrigeration cycle. Heat losses and gains over the compressor, condenser, throttle and evaporator will be calculated, together with the coefficient of performance.



Additionally, a P-h-T chart with the refrigeration cycle will be plotted.

The compressor, condenser, throttle and evaporator are analyzed separately from each other. Calculations are performed by analyzing the specific energy change across each component with this

equation (a statement of the conservation of energy),

$$q - w = \Delta h + \Delta KE + \Delta PE$$

where

- w is the work done by the component
- ΔKE and ΔPE are the changes in kinetic and potential energy
- Δh is the change in specific enthalpy
- q is the heat transferred to the system

Thermophysical properties are provided by the open source C++ CoolProp library (coolprop.org). Once compiled and linked to Maple, CoolProp lets you access the properties of pure fluids, pseudo-pure fluids, and humid air with a function call.

This application comes with a CoolProp DLL for 64-bit Windows. You may need to compile CoolProp on your own computing environment for a compatible library.

While this application uses R134a as the refrigerant, you can investigate the effect of other fluids by replacing references to R134a with your preferred fluid (such as R744).

Load the CoolProp DLL

> restart

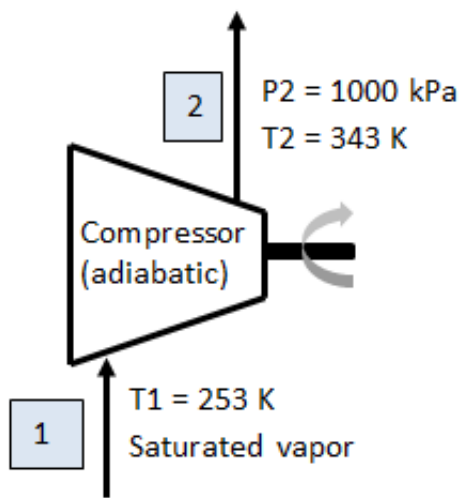
Ensure the path to the DLL is correctly referenced by `define_external()`

```
> Props := define_external( 'Props', LIB = "c:\\CoolProp_x64.dll", 'Output'::string, 'In1'::char, 'Val1'::(float8), 'In2'::char, 'Val2'::(float8), 'Fluid'::string, RETURN::(float8) ) :
```

Valid calling sequences for `Props()` are documented at coolprop.org

Compressor

Consider the energy flows in the compressor. For an adiabatic process, $q = 0$. Also $\Delta KE = 0$ and $\Delta PE = 0$. Hence $-w = \Delta h$



Therefore the enthalpy at points 1 and 2 are (in kJ kg^{-1})

```
> h1 := Props("H", "T", 253, "Q", 1, "R134a")
   h2 := Props("H", "T", 343, "P", 1000, "R134a")
           h1 := 386.461535847473840
           h2 := 451.844244097570993
```

(3.1)

The work done by the compressor (w) is

```
> workCompressor := h1 - h2
           workCompressor := -65.3827083
```

(3.2)

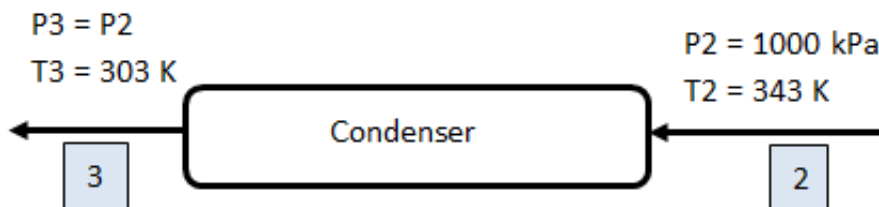
```
> press1 := Props("P", "T", 253, "Q", 1, "R134a")
           press1 := 131.876928437669761
```

(3.3)

```
> press2 := 1000 :
```

Condenser

For the condenser, $w = 0$, $\Delta KE = 0$ and $\Delta PE = 0$. Hence $q = \Delta h$



```
> h3 := Props("H", "T", 303, "P", 1000, "R134a")
           h3 := 241.499519016077613
```

(4.1)

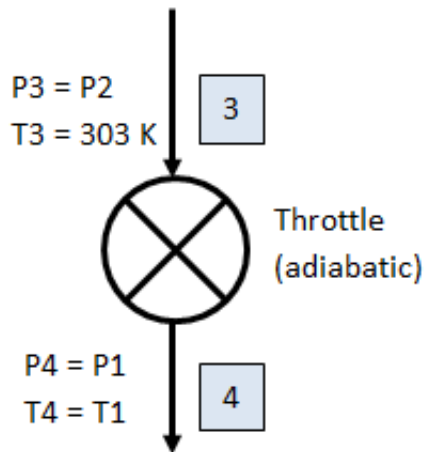
$$> h_3 - h_2$$

$$-210.3447251$$

(4.2)

Throttle

For the throttle, $q = 0$, $w = 0$, $\Delta KE = 0$ and $\Delta PE = 0$. Hence $\Delta h = 0$



Enthalpy at h4

$$> h_4 := h_3$$

$$h_4 := 241.499519016077613$$

(5.1)

Saturation pressure of R134a at 253 K

$$> \text{press4} := \text{press1}$$

$$\text{press4} := 131.876928437669761$$

(5.2)

Quality at $P = \text{press4}$ and $H = h_4$

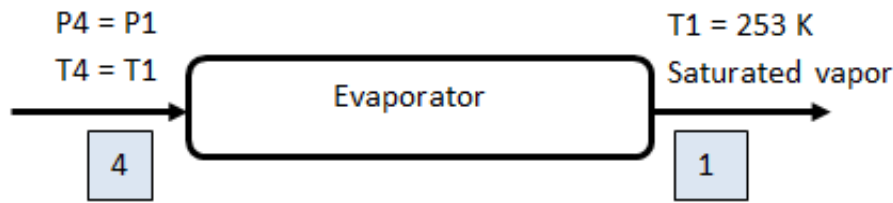
$$> \text{Props}(\text{"Q"}, \text{"P"}, \text{press4}, \text{"H"}, h_4, \text{"R134a"})$$

$$0.319491031236869172$$

(5.3)

Evaporator

For the evaporator, $w = 0$, $\Delta KE = 0$ and $\Delta PE = 0$. Hence $q = \Delta h$



Heat extracted by evaporator

> heatEvaporator := h4 - h1

heatEvaporator := -144.9620168

(6.1)

▼ Coefficient of Performance

> $\frac{\text{heatEvaporator}}{\text{workCompressor}}$

2.217130807

(7.1)

▼ Plot the Refrigeration Cycle on a P-h-T Chart

- > with(plots) :
- > isotherm := contourplot('Props'("T", "H", h, "P", p, "R134a"), h = 150 ..460, p = 60 ..10000, axis₁ = [gridlines = [color = "LightSteelBlue"]], axis₂ = [mode = log, gridlines = [8, subticks = 4, color = "LightSteelBlue"]], contours = [seq(260 + i, i = 0 ..200, 20)], thickness = 0, color = "DarkGray", grid = [150, 150]) :
- > isothermText := textplot([seq([Props("H", "T", 260 + i, "P", 4000, "R134a")], 4000, sprintf("%a K", 260 + i)], i = 0 ..200, 20)], font = [Helvetica, Normal]) :
- > twoPhaseEnvLeft := pointplot([seq([Props("H", "P", i, "Q", 1, "R134a")], i, i = 0 ..4030)], connect = true, thickness = 0) :
- > twoPhaseEnvRight := pointplot([seq([Props("H", "P", i, "Q", 0, "R134a")], i, i = 0 ..4040)], connect = true, thickness = 0) :
- > quality := seq(pointplot([seq([Props("H", "P", p, "Q", q, "R134a")], p, p = 60 ..4000, 100)], connect = true, color = "LightGreen", thickness = 0), q = 0.1 ..0.9, 0.1) :
- > qualityText := textplot([seq([Props("H", "P", 150, "Q", 0.01 · q, "R134a")], 150, sprintf("%a%%", q)], q = 10 ..90, 10)], font = [Helvetica, Normal]) :
- > cycle := pointplot([[h1, press1], [h2, press2], [h3, press2], [h3, press4], [h1, press1]], connect = true, color = "DarkRed", thickness = 2) :
- > display(isotherm, isothermText, twoPhaseEnvLeft, twoPhaseEnvRight, cycle, quality, qualityText, view = [150 ..460, 100 ..5000], title = "P-h-T Chart for R134a", titlefont = [Helvetica, 14], labels = ["Enthalpy (kJ/kg)", "Pressure (kPa)"], labeldirections = [horizontal, vertical], labelfont = [Helvetica, 12])

P-h-T Chart for R134a

